Short communication

# Enhanced rate capability due to highly active $\mathrm{Ta}_{2} \mathrm{O}_{5}$ catalysts for lithium sulfur batteries 

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## HI G H L I G H T S

- Heterogeneous catalysts as reaction intermediates can enhance battery performance.
- $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is one of the most promising heterogeneous catalysts for Li-S battery.
- Strong chemical bonding between S and $\mathrm{Ta}_{2} \mathrm{O}_{5}$ result in catalytic effect of $\mathrm{Ta}_{2} \mathrm{O}_{5}$.
- $\mathrm{Ta}_{2} \mathrm{O}_{5}$ can accelerate slow disproportionation reaction of LiPS.
- Modified separator can help achieving long cycle life and enhanced rate capability.


## ARTICLE INFO

## Keywords:

Lithium-sulfur batteries
Tantalum oxide
Heterogeneous catalyst
Polysulfide
Coated separator

## G R A P H I C A L A B S TRACT




#### Abstract

The heterogeneous catalysis is widely recognized to promote polysulfide fragmentations can play a key role for the rate capability enhancement of lithium sulfur batteries (LSB). In this study, we report the most active catalysts $\left(\mathrm{Ta}_{2} \mathrm{O}_{5}\right)$ for LSB which showed an enhanced rate capability ( $914 \mathrm{mAh}^{-1}$ at 5 C ) in comparison with the previously reported catalysts, $\mathrm{TiN}\left(865 \mathrm{mAh} \mathrm{g}^{-1}\right.$ at 5 C$)$. The addition of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ into the carbon-coated separator facilitates the chemical disproportionation of reaction intermeditates, $\mathrm{Li}_{2} \mathrm{~S}_{4}$ into $\mathrm{Li}_{2} \mathrm{~S}_{8}$ and $\mathrm{Li}_{2} \mathrm{~S}$ effectively, which leads to the greatly lengthened second plateau in discharge profile. The heterogeneous catalysis of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is clearly verified with the UV-Vis spectra directly showing the change of $\mathrm{Li}_{2} \mathrm{~S}_{4}$ concentration and the battery performance tests without any active elemental sulfur.


## 1. Introduction

Lithium sulfur batteries (LSB) is attracting many interests with much higher theoretical capacity ( $1675 \mathrm{mAh} \mathrm{g}^{-1}$ ) and energy density
( $2600 \mathrm{~W} \mathrm{~h} \mathrm{~kg}^{-1}$ ) than conventional lithium ion batteries (LIB) [1-6]. Also, sulfur has many advantages such as natural abundance, low cost, non-toxic and environmental friendliness [7-10]. However, the main drawbacks of LSB are seriously low cyclability due to the dissolution of

[^0]polysulfide, and the slow kinetics leading to low redox activity of sulfur [10-18].

In order to control the dissolution of polysulfide and enhance the conductivity of sulfur, various approaches have been suggested, such as the sulfur impregnation in mesoporous carbon [6,16,19-23], carbon coating [24-28], carbon interlayer [15,29-33], polysulfide absorbents and sulfur catalysts [34-38]. Recently, many attempts for modified separators like using Nafion [39], porous graphene [40], Nano- $\mathrm{TiO}_{2}$ [41], CoP nanosphere [42], Tin sulfide [43] and Conductive MOF [44] for LSB have been studied. The use of modified separators has exhibited good capacity and cycle retention, which could facilitate fast electron or ion transport and inhibit the polysulfide dissolved in the electrolyte [45]. Contrary to the various solutions of low cyclability, the slow kinetics issues have been much less covered in the literature, in which the most common approaches were simple employment of highly conducting carbon material hosts.

A number of literature have reported that using transition metal compounds like sulfides [46-48], oxides [49-51], nitrides [52,53] are effective to enhance cell performance associated with rate capability and cyclability. Most of literature have reported that such additives acted as the effective reservoirs for polysulfides based on their strong affinity to sulfur rather than the electrochemical catalysts to enhance the electrochemical redox reaction by promoting the reactions of polysulfides conversion, as shown in this work.

In our previous report, we suggested a unique solution to improve the slow kinetics and to enhance the rate capability; the heterogeneous catalysis in LSB. The simple addition of TiN facilitated the chemical disproportionation of reaction intermeditates, $\mathrm{Li}_{2} \mathrm{~S}_{4}$ into $\mathrm{Li}_{2} \mathrm{~S}_{8}$ and $\mathrm{Li}_{2} \mathrm{~S}$ effectively, which led to the greatly lengthened second plateau in discharge profile [35]. The role of heterogeneous catalysis was verified using the combined computational and experimental approaches that an ultrastrong adsorption of elemental sulfur on TiN surfaces resulted in a spontaneous fragmentation into shorter chains of polysulfides.

In this study, we introduce a new type of heterogeneous catalyst, $\mathrm{Ta}_{2} \mathrm{O}_{5}$, which played a similar role as TiN , but it demonstrated an increased rate capability compared to TiN. In particular, the combination with $\mathrm{Ta}_{2} \mathrm{O}_{5}$ catalysts and carbon coated separator led to the maximized performance of LSB without any employment of noble carbon hosts which required complex synthetic routes.

## 2. Result and discussion

We begin with the examination of battery performance for LSB having $\mathrm{Ta}_{2} \mathrm{O}_{5}$ added cathode by galvanostatic cycling. First, we examined the electrochemical characteristics of $\mathrm{Ta}_{2} \mathrm{O}_{5}$, prepared by the thermal oxidization of polycrystalline Ta pellet with a tube induction heater in oxygen atmosphere. Fig. 1(a) shows cyclic voltammograms (CV) of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ layer on polycrystalline Ta pellet and glassy carbon (GC) electrode in the sulfur dissolved electrolyte. The GC exhibited characteristic peaks at around 2.0 and 2.4 V (vs. $\mathrm{Li} / \mathrm{Li}^{+}$) in the negative sweep corresponding to the electrochemical reduction from $\mathrm{S}_{8}$ to $\mathrm{Li}_{2} \mathrm{~S}_{8}$ and from $\mathrm{Li}_{2} \mathrm{~S}_{8}$ to $\mathrm{Li}_{2} \mathrm{~S}_{\mathrm{n}}(1 \leq \mathrm{n}<8)$ respectively. On the contrary, the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ demonstrated no characteristic peak like GC, but showed only a slight increase of reduction current, which was attributable to the formation of sulfur passivation layer [35]. The variation of CV with or without sulfur in the electrolyte can be found in the supporting information (Fig. S1). The discharge capacities were examined with $\mathrm{Ta}_{2} \mathrm{O}_{5}$ bare $\left(\mathrm{Ta}_{2} \mathrm{O}_{5}+\right.$ carbon), S bare (sulfur + carbon) and $\mathrm{Ta}_{2} \mathrm{O}_{5}+\mathrm{S}$ (sulfur + carbon $+\mathrm{Ta}_{2} \mathrm{O}_{5}$ ) cathode to understand the role of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ additives. The areal loading of sulfur was $1 \mathrm{mg} / \mathrm{cm}^{2}$, and its size was about $4-10 \mu \mathrm{~m}$ on electrode as in Fig. S2. At first, no discharge capacity was observed for the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ bare as expected in the CV for polycrystalline $\mathrm{Ta}_{2} \mathrm{O}_{5}$ layer without sulfur (Fig. S3). This implies that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ in itself has no activity for the electrochemical reduction of sulfur and also no capacity for lithium intercalation. $\mathrm{Ta}_{2} \mathrm{O}_{5}+\mathrm{S}$ however showed a superior performance to $S$ bare in general as in Fig. 1(b). It is interesting


Fig. 1. (a) CV curves of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ layer on polycrystalline Ta pellet and GC electrode. (b) Discharge capacity of S bare and $\mathrm{Ta}_{2} \mathrm{O}_{5}+\mathrm{S}$ cathode in various C-rates.
to note that the difference of discharge capacity for two kinds of cathodes is marginal in low C-rate, while it becomes larger drastically in high C-rate region. In particular, the discharge capacity of $\mathrm{Ta}_{2} \mathrm{O}_{5}+\mathrm{S}$ is about 3 times higher than S bare in 5 C , indicating that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ additives are selectively effective on the enhancement of rate capability for high C-rate. This is attributable to the fact that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ possesses no electrochemical activity to the sulfur reduction reaction but the heterogeneous catalytic activity to the chemical disproportionation reaction as we reported in the former literature [35]. In our previous work, TiN acted as a heterogeneous catalyst to promote the fragmentation of lithium polysulfide. This unique phenomenon was attributed to the ultrastrong chemical bonding between S and TiN surface. The S-passivated TiN surfaces provided the suitable sites for the stabilization of short-chain lithium polysulfides and the fragmentation of long-chain ones into shorter chains. Hence, it was hypothesized that the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ also acted as heterogeneous catalysts similar to the case of TiN.

In order to verify this hypothesis, we carried out some experiments like XPS studies on $\mathrm{Ta}_{2} \mathrm{O}_{5}$ surfaces exposed to the elemental sulfur, and UV-Vis spectroscopy to observe the chemical disproportionation on $\mathrm{Ta}_{2} \mathrm{O}_{5}$ surfaces. In our previous work, we reported that the elemental sulfur is unstable on the TiN surface, allowing the $\mathrm{Ti}-\mathrm{S}$ bond primarily [35]. In this context, we examined the interaction between sulfur and $\mathrm{Ta}_{2} \mathrm{O}_{5}$ by XPS. As shown in Fig. 2(a) with our previous work [35], the binding energy of the S 2 p electron in the elemental $\mathrm{S}_{8}$ was observed 164.09 eV . However, the S 2 p electron in the toluene-washed $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{S}$ composite shifts from 164.09 eV to 162.57 eV shown in Fig. 2(b). This shift can be ascribed to the increased electron density around the S atoms, as shown in the various metal sulfides [54]. Consequently, $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is expected to outperform other host materials like TiN ( -0.99 eV ) [35]


Fig. 2. XPS $2 p$ spectra of (a) elemental sulfur and (b) $\mathrm{S}_{8}$ on $\mathrm{Ta}_{2} \mathrm{O}_{5}$.
and WC ( -0.72 eV ) [55] in our previous works. Furthermore, the peak around 169 eV is commonly known as the $\mathrm{S}-\mathrm{O}$ band [56,57], which was produced by the interaction between S and O from $\mathrm{Ta}_{2} \mathrm{O}_{5}$. This may be another evidence that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ and sulfur interact strongly, associated with other experimental results. Hence, this result strongly suggests that the surface-bound $\mathrm{S}_{8}$ rings are fully disrupted forming chemical bonds between sulfur and $\mathrm{Ta}_{2} \mathrm{O}_{5}$, indicating the formation of passivation layer. Thereby $\mathrm{Ta}_{2} \mathrm{O}_{5}$ might played an important role as heterogeneous catalysts similar to the TiN. On the contrary, the intensity of the spectra for sulfur on carbon (Fig. S4) was much lower than that for $\mathrm{Ta}_{2} \mathrm{O}_{5}$, and was hard to detect the peak shift. This indicates that the formation of passivation layer between carbon and sulfur is negligible compared to $\mathrm{Ta}_{2} \mathrm{O}_{5}$ and sulfur, thus the unique interaction in the sulfur passivated $\mathrm{Ta}_{2} \mathrm{O}_{5}$ surface plays an essential role in enhancing the battery performance.

Besides, XPS for $\mathrm{Ta}_{2} \mathrm{O}_{5}$-polysulfide mixture shows that the S 2 p peak was shifted -1.91 eV compared to elemental sulfur (Fig. S5). Also comparing the intensity of 169 eV , it is much stronger in $\mathrm{Ta}_{2} \mathrm{O}_{5}$-polysulfide than in $\mathrm{Ta}_{2} \mathrm{O}_{5}-\mathrm{S}$, means that much stronger $\mathrm{S}-\mathrm{O}$ band is formed in the case of $\mathrm{Ta}_{2} \mathrm{O}_{5}$-polysulfide. Thus, it confirmed that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ forms ultrastrong chemical bonding not only with sulfur but also with polysulfide and has especially stronger interaction with polysulfide.

The heterogeneous catalysis on $\mathrm{Ta}_{2} \mathrm{O}_{5}$ surfaces was clearly verified with the in-situ UV-Vis spectroscopy. $\mathrm{Li}_{2} \mathrm{~S}_{4}$ was synthesized according to the previous literature and was dissolved in the electrolyte [35,49]. Then, a chronoamperometric (CA) measurement was performed at 2.0 V vs. $\mathrm{Li} / \mathrm{Li}^{+}$for a given period of time with a RDE setup potentiostat. GC and $\mathrm{Ta}_{2} \mathrm{O}_{5}$ pellet were used as a working electrode as Fig. 1, and the lithium metal was used as both the reference and counter electrodes. As shown in Fig. 3, while the peak intensity at around lambda $=410 \mathrm{~nm}$ (corresponding to the $\mathrm{Li}_{2} \mathrm{~S}_{4}$ concentration) for the GC showed little
difference with reaction time, the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ exhibited a notable decrease of peak height as well as the color change of the electrolyte. Also, in the case of $\mathrm{Ta}_{2} \mathrm{O}_{5}$, yellow-white powder precipitate was formed inside the electrolyte and on the electrode surface. It was found to be sulfur (Fig. S6), which was formed by the disproportionation reaction of $\mathrm{Li}_{2} \mathrm{~S}_{4}$, implying that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ promotes the polysulfide disproportionation reaction. As a result, the heterogeneous catalysis on $\mathrm{Ta}_{2} \mathrm{O}_{5}$ surface was clearly confirmed with two strong evidences like the sulfur binding energy shift in XPS and the absorption peak intensity decrease in UV-Vis spectroscopy.

In our previous studies, we demonstrated that the combination of heterogeneous catalysis with polysulfide capture techniques like carbon interlayers having a large electrochemically active surface area is an effective approach to enhance the performance of LSB and to decrease the production cost of LSB with a simple insertion of the catalyst and carbon coated separator [30,35]. To maximize the cell performance, we prepared the $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator via a simple casting and drying of ink composed of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ and carbon in the PvdF-contained solvent onto the PE separator. The morphology of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ powder and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator with scanning electron microscopy (SEM) and energy dispersive spectrometer (EDS) are shown in Fig. S7. The particle size of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is around $1 \mu \mathrm{~m}$ from the SEM images and the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ and carbon are homogenously mixed on the separator from the EDS spectra. Electrochemical impedance spectroscopy (EIS) measurements were performed on bare and $\mathrm{Ta}_{2} \mathrm{O}_{5}$ electrodes from 100 mHz to 1 MHz region to verify the catalytic promotion of chemical disproportionation by $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is responsible for the superior performance of LSB (Fig. S8). At the high frequency region, the impedance response shows a semicircular loop, which is relevant to the charge transfer resistance, a measure of the charge transfer kinetics. As a result, it was clearly observed that the charge transfer resistance of the cell with $\mathrm{Ta}_{2} \mathrm{O}_{5}$ decreases dramatically and is lower than that of the cell of the bare electrode. This indicates that the catalysis of the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ can improve the electrochemical kinetics of LSB [58].

In order to confirm the effect of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ catalysts in the $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator, we compared the battery performances among the LSBs with $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator, carbon coated separator (C separator) and conventional polyethylene separator (PE separator). Fig. 4 shows the chargedischarge profiles and the cycle performances on different C-rates, and CV for the cells having different kinds of separators. All the cells showed typical voltage profiles for LSB having two plateaus at around 2.4 V and 2.0 V , which was corresponding to the formation of dissolvable lithium polysulfide $\left(\mathrm{Li}_{2} \mathrm{~S}_{\mathrm{n}}, 4 \leq \mathrm{n} \leq 8\right)$ and perceptible lithium sulfide $\left(\mathrm{Li}_{2} \mathrm{~S}_{\mathrm{n}}\right.$, $\mathrm{n} \leq 2$ ), respectively $[14,59,60$ ]. Compared to the PE separator, C and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator showed an enhanced battery performance. The discharge capacities of $\mathrm{PE}, \mathrm{C}$ and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator were 606,951 , $1108 \mathrm{mAh} \mathrm{g}^{-1}$ at 0.5 C (Fig. 4(a)) and 129, 755, $914 \mathrm{mAh} \mathrm{g}^{-1}$ at 5 C (Fig. 4(b)). Generally, at high C-rate, the iR resistance increases, so compared to the curve at 0.5 C , the ohmic loss is serious at 5 C , so that the second plateau does not appear in PE separator. Also, during the discharging process, since the very sluggish chemical disproportionation reaction requires an enough time to proceed the reaction, however, under the high C-rate like 5 C , there is not enough time to form the second plateau by supplying polysulfide intermediate due to the chemical disproportionation, which increase the effect of the ohmic loss. In the case of $C$ separator, it is obvious that the resistance is reduced by the effect of reaction area increase due to carbon particles on the separator. Hence, the second plateau in the discharge curve can be observed in contrast with the PE separator. In particular, for the $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator, since the catalyst also promotes the sluggish chemical disproportionation, the second plateau is clearly observed. The results for other C-rates like 1 C or 2C are shown in Fig. S9. This indicates that the modified separator is obviously effective to enhance the battery performance and particularly the rate capability. Indeed, there have been several reports that modified separator such as carbon coated separator resulted in the performance enhancement of LSB. In the previous literature, it was already reported that the carbon coated separator


Fig. 3. UV/Vis spectra measured in operando mode using a rotating disk electrode with (a) carbon-pellet and (b) $\mathrm{Ta}_{2} \mathrm{O}_{5}$-pellet in the electrolyte containing 30 mM $\mathrm{Li}_{2} \mathrm{~S}_{4}$. (c) Visual confirmation of polysulfide disproportionation by concentration change of electrolyte with $\mathrm{Li}_{2} \mathrm{~S}_{4}$ before and after test with $\mathrm{GC}^{\text {and }} \mathrm{Ta}_{2} \mathrm{O}_{5}$.
could capture the polysulfide dissolved in electrolyte [61]. It is however interesting to note here that the separator with $\mathrm{Ta}_{2} \mathrm{O}_{5}$ demonstrated markedly enhanced battery performance at all the tested C-rates. In particular, the capacity difference between $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator and others became greater with the increase of C-rate, implying that the rate capability was drastically enhanced by the addition of $\mathrm{Ta}_{2} \mathrm{O}_{5}$. Also, $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator showed smaller polarizations than the other samples at a high C-rate. On the side of cyclability, the $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator exhibited good capacity retention (Fig. 4(c)). After 100 cycles, the capacities of PE, C and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator were 375,786 and 964 mAh $\mathrm{g}^{-1}$, which the capacity retention of $54.3 \%, 76.6 \%$ and $81.9 \%$ based on the 10th cycle, and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator also show a good cycle performance in higher C-rate like 2 C (Fig. S10). Moreover, in high sulfur loading ( $5.91 \mathrm{mg} / \mathrm{cm}^{2}$ ), the 0.2 C cycle characteristics result in high coulombic efficiency of $99.9 \%$ at 5th cycle, and also $92.8 \%$ was maintained even in the 50th cycle (Fig. S11). Therefore, it shows that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is also capable for high sulfur loading.

In order to clearly manifest the origin of markedly enhanced rate capability by $\mathrm{Ta}_{2} \mathrm{O}_{5}$ addition, we carried out the CV measurements with the battery cells. As shown in Fig. 4(d), the CV curves for the cells with PE, C and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator demonstrated a typical characteristic of LSB having two peaks in both positive and negative sweep. The negative peaks at 2.4 V and 2.0 V were widely recognized to be corresponding of the transformation of sulfur to long-chain soluble lithium polysulfide and reduction of lithium polysulfide to insoluble lithium sulfide,
respectively. The positive peak at 2.5 V indicated the formation of sulfur from the discharge products $\left(\mathrm{Li}_{2} \mathrm{~S}\right)$, which was well consistent with the charge-discharge voltage profiles. Even though the CV for $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator showed also typical redox peaks, there is a notable point in the negative sweep that the intensity of second wave and the ratio of second wave to first wave are much higher than any other cells. In C separator, there will be no kinetic enhancement or catalytic effect to promote cell performance because it was used only carbon and no catalyst to make modified separator. Therefore, only the increase of the intensity or the CV area was occurred by the increase of the reaction area, while in $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator shows not only a considerable increase in the capacity consistent with the higher discharge capacity but the peak shift compared to other electrodes. Such difference indicates that LSB with $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator has a better ability to reduce polysulfide than C and PE separator, because the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ in the $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator acted as a heterogeneous catalyst to promote the chemical disproportionation reaction of reaction intermediates like $\mathrm{Li}_{2} \mathrm{~S}_{4}$ which requires a relatively long time to proceed and therefore can be attributed to the main origin of poor rate capability of LSBs. Similar phenomenon also occurred with the CV curve using a composite cathode cell containing $10 \mathrm{w} \% \mathrm{Ta}_{2} \mathrm{O}_{5}$ shown in Fig. S12, indicating $\mathrm{Ta}_{2} \mathrm{O}_{5}$ lowers the activation energy and thus increases the kinetics of reactions.

Also, a simple comparison was made with our previously reported TiN under the same conditions. In Fig. $\mathrm{S} 13, \mathrm{Ta}_{2} \mathrm{O}_{5}$ shows similar or better performance than TiN , indicates that $\mathrm{Ta}_{2} \mathrm{O}_{5}$ also possesses


Fig. 4. Charge-discharge profiles at (a) 0.5 C , (b) 5 C . (c) Cyclability of the $\mathrm{PE}, \mathrm{C}, \mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator at 0.2 C . (d) CV curves of PE , C and $\mathrm{Ta}_{2} \mathrm{O}_{5} / \mathrm{C}$ separator at a scan rate of $0.1 \mathrm{mV} / \mathrm{s}$.
excellent catalytic activity for chemical disproportionation. Hence, we strongly suggest that the employment of heterogeneous catalysts possessing an activity for chemical disproportionation of polysulfides as reaction intermediates is essential for battery performance enhancement and particularly the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ is one of the most promising materials for the heterogeneous catalysts in LSBs.

## 3. Conclusions

In summary, we have suggested a simple and unique approach to enhance the electrochemical properties of LSB using the heterogeneous catalyst coated separator. The catalyst coated separator possessed many useful characteristics with synergistic effects that were responsible for the enhanced capacities and cyclic stability. LSB with $\mathrm{Ta}_{2} \mathrm{O}_{5}$ coated separator displayed on an excellent discharge capacity of $964 \mathrm{mAh} \mathrm{g}^{-1}$ and a good cycle retention of $81.9 \%$ after 100 cycles. It also delivered an excellent discharge capacity of $914 \mathrm{mAh}^{-1}$ at 5 C . We discovered that heterogeneous catalysis to promote the fragmentation of polysulfides, based on the ultra-strong adsorption on $\mathrm{Ta}_{2} \mathrm{O}_{5}$ can markedly enhance the discharge capacity and rate capability of LSB. The catalytic properties of $\mathrm{Ta}_{2} \mathrm{O}_{5}$ were revealed to be the ultra-strong chemical bonding between S and the $\mathrm{Ta}_{2} \mathrm{O}_{5}$ surfaces using the experimental analysis. This simple strategy of coating separator could aid in achieving long cycle life and enhanced rate capability for future commercialization of LSB.

## Acknowledgement

This work was supported by the grant of National Research Foundation (2018R1A2A1A05079375, 2018M1A2A2063167, 2017R1A4A1015533, 2015M1A2A2056556, 2014M1A8A1049348), and the institutional program of the Korea Institute of Science and Technology (2E29641).

## Appendix A. Supplementary data

Supplementary data to this article can be found online at https://doi. org/10.1016/j.jpowsour.2019.226707.

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    https://doi.org/10.1016/j.jpowsour.2019.226707
    Received 25 March 2019; Received in revised form 18 May 2019; Accepted 30 May 2019
    Available online 22 June 2019
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